This article was downloaded by:
On: 25 January 2011
Access details: Access Details: Free Access
Publisher Taylor \& Francis
Informa Ltd Registered in England and Wales Registered Number: 1072954 Registered office: Mortimer House, 3741 Mortimer Street, London W1T 3JH, UK


## Journal of Macromolecular Science, Part A

Publication details, including instructions for authors and subscription information:
http://www.informaworld.com/smpp/title $\sim$ content=t713597274

## Conversion of Fumarate Double Bonds in Unsaturated Polyester Resins in Copolymerization with Styrene

## Kahei Sakaguchiab; Hirotaka Takemoto ${ }^{\text {a }}$

${ }^{\text {a }}$ Kao-Atlas Laboratories 1334 Minatoyakushubata Wakayama-Shi, Japan ${ }^{\text {b }}$ Kao Soap Co., Ltd., Tokyo, Japan

To cite this Article Sakaguchi, Kahei and Takemoto, Hirotaka(1976) 'Conversion of Fumarate Double Bonds in Unsaturated Polyester Resins in Copolymerization with Styrene', Journal of Macromolecular Science, Part A, 10: 6, 1117 - 1141

To link to this Article: DOI: 10.1080/00222337608061240
URL: http://dx.doi.org/10.1080/00222337608061240

## PLEASE SCROLL DOWN FOR ARTICLE

```
Full terms and conditions of use: http://www.informaworld.com/terms-and-conditions-of-access.pdf
This article may be used for research, teaching and private study purposes. Any substantial or
systematic reproduction, re-distribution, re-selling, loan or sub-licensing, systematic supply or
distribution in any form to anyone is expressly forbidden.
The publisher does not give any warranty express or implied or make any representation that the contents
will be complete or accurate or up to date. The accuracy of any instructions, formulae and drug doses
should be independently verified with primary sources. The publisher shall not be liable for any loss,
actions, claims, proceedings, demand or costs or damages whatsoever or howsoever caused arising directly
or indirectly in connection with or arising out of the use of this material.
```


# Conversion of Fumarate Double Bonds in Unsaturated Polyester Resins in Copolymerization with Styrene 

KAHEI SAKAGUCHI* and HIROTAKA TAKEMOTO

## ABSTRACT

Several varieties of unsaturated polyester resins were prepared to investigate the effect of chemical structure and molecular weight and the initial mole fraction of styrene on the conversion of fumarate double bond in the copolymerization with styrene.
The conversion of the fumarate double bond was calculated from the soluble portion of polyester resin, according to the theoretical equations which were proposed in a previous paper. Conversion first increased with increasing initial mole fraction of styrene. At an initial mole fraction of styrene higher than 0.6-0.7, however, the conversion of fumate double bond decreased.
Styrene homopolymer was separated from the soluble material by elution chromatography on a silica gel-packed

[^0]
#### Abstract

column. The purity of polyester component in the soluble part of the polyester resin was determined by infrared spectroscopy and by the saponification number. The conversion of fumarate double bond was calibrated by using corrected values of the soluble part of polyester resin. The chemical structure and the molecular weight of unsaturated polyester resins also affect the conversion of fumarate double bond. In Bisphenol-type resins, the conversion of fumarate double bond increased with the extension of polyoxypropylene unit attached to Bisphenol A, and the increase of the molecular weight of primary polyester resin was unfavorable for the conversion of fumarate double bond. In a series of propylene glycol fumarate resins, the adipic acid-modified resin gave a higher conversion of fumarate double bond than the isophthalic acid-modified resin and the phthalic acid-modified resin. The polyester resin prepared from chlorendic anhydride gave the lowest conversion of fumarate double bonds among the polyester resins investigated in the present paper. The extent of conversion of fumarate double bond may be restricted by the properties of the network such as rigidity, the crosslinking density, and steric hindrance of groups like chlorine.


## INTRODUCTION

The mechanical, electrical, and chemical properties of polyester resins are related to the degree of cure of the resin. Many investigators have tried to determine the degree of cure by means of physical and chemical methods. The degree of cure has been expressed by the conversion of styrene and fumarate double bonds. The conversion of styrene can be easily determined by solvent extraction of the powdered resins, with subsequent analysis of styrene by using either ASTM Method D-1159, the bromine index method, or gas chromatography. On the other hand, the conversion of fumarate double bond is difficult to determine. Funke et al. [1-5] and other investigators [6-8] have used the alkaline hydrolysis method for the determination of the conversion of fumarate double bond. They hydrolyzed the cured polyester resin by alkall and analyzed the residue by elemental analysis and infrared spectroscopy.

Previously, one of the present authors [9] presented a paper on the determination of the conversion of fumarate double bonds which were crosslinked into three-dimensional polymers. The experiments
were based on the chloroform extraction of the crosslinked resin. The conversion of fumarate double bond was calculated from the soluble portion of polyester resin by using theoretical equations derived from the basic theory of Flory [10].

In the present paper, factors affecting the conversion of fumarate double bonds in unsaturated polyester resins were investigated. Several varieties of unsaturated polyester resins including Bisphenoltype, iso-type, G-type, and Het acid-type resins were prepared with varying chemical compositions, molecular weight of the primary polyester resin, and the initial concentration of styrene.

## EXPERIMENTAL

All unsaturated polyester resins were prepared in a four-necked, round-bottomed, 5 -liter flask kettle equipped with a stirrer, nitrogen gas inlet, thermometer, and distillation head. When glycols of relatively low boiling point such as propylene glycol and neopentyl glycol were esterified, a distillation head packed with stainless steel mesh packings was used to enhance the efficiency in separation of the water from the glycols. Esterification was usually carried out in one step, but a two-step process was used for iso-type resin. Reaction mixtures including 400 ppm of hydroquinone as inhibitor were charged into the kettle and heated by a mantle with a stream of nitrogen gas during the esterification. The reaction was carried out at the temperatures from 140 to $210^{\circ} \mathrm{C}$ to appropriate molecular weight. Several varieties of the resins were prepared.

## Bisphenol-Type Resin

The standard resin in Bisphenol-type resin is a condensate of propoxylated ( 2.2 mole) Bisphenol $A$ and fumaric acid. The resins having the different degrees of esterification were prepared by changing the reaction time. To change the average molecular weight between the two fumarate units, the resin was modified by extending the propoxylate unit adducted to Bisphenol A, and incorporating neopentyl glycol, propylene glycol, hydrogenated Bisphenol A and $\beta$-hydroxyethyl terephthalate as a glycol component, and succinic acid and adipic acid as a dibasic acid component.

G-Type, Iso-Type, and Het Acid-Type Resins
Propylene glycol fumarate is the standard resin in G-type resins. The only modifications made were in the acid components, different
amounts of phthalic anhydride and adipic acid being used to prepare the resin having the various average molecular weight between the two fumarate units. An iso-type resin and a Het acid-type resin were prepared by using isophthalic acid and Het-acid (chlorendic anhydride), respectively.

The unsaturated polyester resins prepared were characterized by acid number, hydroxyl number and saponification number. The equivalents of fumarate double bonds and the average molecular weight between the two fumarate units, $\overline{\mathrm{M}}_{0}$, were calculated from the composition charged. The number-average molecular weight for the polyesters, $\bar{M}_{\mathrm{n}}$, was determined by endgroup analysis, acid number, and hydroxyl
number. The resins thus obtained were dissolved in styrene at an appropriate concentration at room temperature. Polyester-styrene solutions were cured with a catalyst mixture of $0.1 \%$ dimethylaniline, $0.5 \%$ cobalt naphthenate (as a $6 \%$ solution) and $1 \%$ methyl ethyl ketone peroxide (as a $55 \%$ solution). The catalyzed resin solution was poured into a mold consisting of two plates of glass which were covered with polyester film and sepearated by a 4 mm poly(vinyl chloride) spacer, and the resin was allowed to cure at room temperature for 24 hr . The castings were then placed in an oven at $100^{\circ} \mathrm{C}$ for 2 hr for completion of the cure.

The cured resins were rasped with steel file with slow, steady strokes to prevent overheating, and 10 g of powdered resin was extracted three times with 300 g of chloroform. The resin-solvent mixture was filtered off for each extraction. The extract solution was analyzed for unreacted styrene which was satisfactorily determined by gas chromatography method. The solutions were then evaporated on a steam bath and dried in vacuo at $100^{\circ} \mathrm{C}$. The resins extracted from the cured resin were subjected to further analysis by elution chromatography of silica gel-packed column, acid number, hydroxyl number, saponification number, gel permeation chromatography, and infrared spectroscopy.

## RESULTS AND DISCUSSION

The results for the various polyester resins are summarized in Tables 1-3. The initial concentration of styrene in the polyester resin solution is $50 \pm 0.5 \mathrm{wt} \%$ for all resins, so the initial mole fraction of styrene, $\mathrm{f}_{\mathrm{S}_{0}}$, for each polyester resins varies with the average molecular weight between two fumarate units, $\overline{\mathbf{M}}_{0}$.

The conversion of styrene $\mathbf{C}_{\mathrm{S}}$ is above $90 \%$ for all resins. The
table 1. Chemical Characteristics of Various Polyester Resins

|  |  |  | Unsaturated polyester resin |  |  |  |  |  |  |  | Styrene |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Expt. <br> no. | Resin no. | Type | Composition (mole ratio) ${ }^{\text {a }}$ | Fumarate <br> double <br> bond $(e q / 100 \mathrm{~g})$ | $\overline{\mathbf{M}}_{0}$ | Acid no. | Hydrox- <br> yl no. | Saponification no. | $\overline{\mathbf{M}}_{\mathbf{n}} \mathbf{b}$ | $\bar{x} c$ | wt \% | $\begin{aligned} & \mathrm{f}_{\mathrm{S}_{0}} \\ & \text { (mole } \\ & \text { fraction) } \end{aligned}$ |
| 1 | B(2)-1 | Bisphenol | $\begin{aligned} & \mathrm{B}(2) / \mathbf{F A} \\ & =1 / 1 \end{aligned}$ | 0.219 | 456 | 4.4 | 23.4 | 248.7 | 4040 | 8.9 | 49.7 | 0.812 |
| 2 | B(2)-2 | Bisphenol | $\begin{aligned} & B(2) / F A \\ & =1 / 1 \end{aligned}$ | 0.219 | 456 | 7.8 | 26.2 | 243.8 | 3300 | 7.2 | 50.0 | 0.814 |
| 3 | B(2)-4 | Bisphenol | $\begin{aligned} & B(2) / F A \\ & =1 / 1 \end{aligned}$ | 0.219 | 456 | 11.9 | 28.3 | 250.0 | 2794 | 6.1 | 50.0 | 0.814 |
| 4 | B(2)-5 | Bisphenol | $\begin{aligned} & \mathrm{B}(2) / \mathrm{FA} \\ & =1 / 1 \end{aligned}$ | 0.219 | 456 | 11.9 | 30.1 | 242.9 | 2672 | 5.9 | 50.0 | 0.814 |
| 5 | B(2)-6 | Bisphenol | $\begin{aligned} & B(2) / F A \\ & =1 / 1 \end{aligned}$ | 0.219 | 456 | 25.4 | 28.6 | 259.1 | 2078 | 4.6 | 50.0 | 0.814 |
| 6 | B(2)-7 | Bisphenol | $\begin{aligned} & B(2) / F A \\ & =1 / 1 \end{aligned}$ | 0.219 | 456 | 30.8 | 33.7 | 255.4 | 1740 | 3.8 | 50.0 | 0.814 |
| 7 | B(2)-8 | Bisphenol | $\begin{aligned} & B(2) / F A \\ & =1 / 1 \end{aligned}$ | 0.219 | 456 | 19.0 | 60.1 | 227.1 | 1419 | 3.1 | 49.8 | 0.813 |
| 8 | B(2)-9 | Bisphenol | $\begin{aligned} & B(2) / F A \\ & =1 / 1 \end{aligned}$ | 0.219 | 456 | 22.8 | 81.9 | 213.3 | 1072 | 2.4 | 49.7 | 0.812 |
| 9 | B(5) | Bisphenol | $\begin{aligned} & B(5) / F A \\ & =1 / 1 \end{aligned}$ | 0.174 | 586 | 22.4 | 26.4 | 169.7 | 2300 | 3.9 | 50.2 | 0.850 |
| 10 | B(9) | Bisphenol | $\begin{aligned} & \mathrm{B}(9) / \mathrm{FA} \\ & =1 / 1 \end{aligned}$ | 0.214 | 809 | 21.5 | 31.8 | 136.2 | 2105 | 2.6 | 50.0 | 0.886 |
| 11 | B(15) | Bisphenol | $\mathrm{B}(15) / \mathrm{FA}-1 / 1$ | 0.086 | 1158 | 12.9 | 41.1 | 90.6 | 2078 | 1.8 | 50.0 | 0.918 |
| 12 | BM-NG-1 | Bisphenol | $\begin{aligned} & \mathrm{B}(2) / \mathrm{NPG} / \mathrm{FA} \\ & =1 / 1 / 2 \end{aligned}$ | 0.321 | 312 | 10.5 | 62.7 | 316.0 | 1533 | 4.9 | 50.1 | 0.750 |
| 13 | BM-PG-2 | Bisphenol | $\begin{aligned} & \mathrm{B}(2) / \mathrm{PG} / \mathrm{FA} \\ & =1 / 1 / 2 \end{aligned}$ | 0.339 | 295 | 22.5 | 30.8 | 371.4 | 2105 | 7.1 | 49.9 | 0.738 |
| 14 | BM-MB-1 | Bisphenol | $\begin{aligned} & \mathrm{B}(2) / \mathrm{HBPA} / \mathrm{FA} \\ & =1 / 1 / 2 \end{aligned}$ | 0.264 | 378 | 28.2 | 31.8 | 285.5 | 1870 | 5.0 | 49.5 | 0.781 |

TABLE 1 (continued)

| Expt.no. | Resin no. | Type | Unsaturated polyester resin |  |  |  |  |  |  |  | Styrene |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  |  | Composition (mole ratio) ${ }^{\text {a }}$ | Fumarate double bond (eq/100 g) | $\overline{M_{0}}$ | Acid <br> no. | Hydroxyl no. | Saponification no. | $\bar{M}_{\mathbf{n}}{ }^{\text {b }}$ | $\bar{x}^{\mathbf{c}}$ | wt \% | ${ }^{f} \mathrm{~S}_{\text {。 }}$ <br> (mole <br> fraction) |
| 15 | BM-HETPA | Bisphenol | $\begin{aligned} & \mathrm{B}(2) / \mathrm{HETPA} / \mathrm{FA} \\ & =1 / 1 / 2 \end{aligned}$ | 0.260 | 384 | 26.5 | 30.1 | 415.9 | 2400 | 5.2 | 50.1 | 0.787 |
| 16 | BM-SA-1 | Bisphenol | $\begin{aligned} & \mathrm{B}(2) / \mathrm{SA} / \mathrm{FA} \\ & =3 / 1 / 2 \end{aligned}$ | 0.151 | 661 | 20.6 | 33.2 | 250.3 | 2086 | 3.2 | 49.7 | 0.863 |
| 17 | BM-SA-2 | Bisphenol | $\begin{aligned} & \mathrm{B}(2) / \mathrm{SA} / \mathrm{FA} \\ & =2 / 1 / 1 \end{aligned}$ | 0.116 | 862 | 21.9 | 31.3 | 249.7 | 2109 | 2.5 | 49.9 | 0.892 |
| 18 | BM-AA-1 | Blisphenol | $\begin{aligned} & \mathrm{B}(2) / \mathrm{AA} / \mathrm{FA} \\ & =3 / 1 / 2 \end{aligned}$ | 0.148 | 675 | 12.8 | 29.9 | 240.2 | 2628 | 3.9 | 50.2 | 0.867 |
| 19 | BM-AA-2 | Bisphenol | $\begin{aligned} & B(2) / \mathrm{AA} / \mathrm{FA} \\ & =2 / 1 / 1 \end{aligned}$ | 0.110 | 911 | 20.3 | 31.8 | 239.7 | 2154 | 2.4 | 50.0 | 0.897 |
| 20 | IPA | Iso | $\begin{aligned} & \text { PG/IPA/FA } \\ & =3.3 / 2 / 1 \end{aligned}$ | 0.169 | 591 | 24.7 | 39.9 | 575.7 | 1740 | 2.9 | 50.4 | 0.853 |
| 21 | G-1 | G | PG/FA $=1.05 / 1$ | 0.641 | 156 | 22.8 | 38.5 | 674.8 | 1831 | 11.7 | 50.2 | 0.601 |
| 22 | G-2 | G | $\begin{aligned} & \text { PG/PA/FA } \\ & =1.47 / 0.33 / 1.0 \end{aligned}$ | 0.415 | 241 | 17.2 | 44.1 | 628.6 | 1831 | 7.6 | 50.1 | 0.699 |
| 23 | G-3 | G | $\begin{aligned} & \mathrm{PB} / \mathrm{PA} / \mathrm{FA} \\ & =3.3 / 1 / 2 \end{aligned}$ | 0.369 | 271 | 25.4 | 49.5 | 608.8 | 1498 | 5.5 | 49.7 | 0.720 |
| 24 | G-4 | G | $\begin{aligned} & \mathrm{PG} / \mathrm{PA} / \mathrm{FA} \\ & =2.2 / 1 / 1 \end{aligned}$ | 0.265 | 378 | 19.3 | 45.9 | 589.4 | 1721 | 4.6 | 49.8 | 0.783 |
| 25 | G-5 | G | $\begin{aligned} & \mathrm{PG} / \mathrm{PA} / \mathrm{FA} \\ & =3.3 / 2 / 1 \end{aligned}$ | 0.169 | 591 | 16.7 | 42.6 | 565.0 | 1892 | 3.2 | 50.0 | 0.850 |
| 26 | G-7 | G | $\begin{aligned} & \text { PG/AA/FA } \\ & =3.3 / 2 / 1 \end{aligned}$ | 0.181 | 552 | 21.7 | 34.2 | 613.7 | 2007 | 3.6 | 50.0 | 0.841 |
| 27 | G-8 | G | $\begin{aligned} & \text { PG/AA/FA } \\ & =4.4 / 3 / 1 \end{aligned}$ | 0.134 | 746 | 24.3 | 34.4 | 620.0 | 1910 | 2.6 | 50.0 | 0.877 |
| 28 | G-9 | G | $\begin{aligned} & \text { PG/AA/FA } \\ & =5.5 / 4 / 1 \end{aligned}$ | 0.106 | 940 | 23.0 | 35.1 | 598.0 | 1931 | 2.1 | 50.0 | 0.900 |

옹
HETA
NPG/HETA/FA 0.246
.
$406=29.1$
8
8
8
0
4
4
4
4
4
4
4
4
4
HET-Acid
406.6
0.796

会


.


| Analysis of polyester resins extracted |  |  |  |  |  |  |  |  | Purity of polyester component |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Expt. no. | $\begin{aligned} & \text { Cs } \\ & \text { (mole } \\ & \text { \%) } \end{aligned}$ | $\begin{aligned} & W_{0} \\ & \text { (mole } \\ & \text { © }) \end{aligned}$ | qo (mole \%) |  |  |  | $\overline{\mathrm{M}}_{\mathrm{SOL}}$ | $\overline{\mathrm{M}}_{\mathrm{SOL}}$ |  |  |
|  |  |  |  | no. | yl no. | cation no. | EGA) | GPC) | By $\mathbf{I R}$ | By |
| 1 | 98.9 | 3.76 | 39 | 20.2 | 87.1 | 145 | 1046 | 888 | 59 | 58. |
| 2 | 99.1 | 3.48 | 47 | 13.3 | 62.2 | 142 | 1486 | 725 | 60 | 58. |
| 3 | 98.0 | 2.50 | 59 | 13.8 | 113.0 | 144 | 885 | 1284 | 51 | 58. |
| 4 | 98.0 | 3.64 | 53 | 17.1 | 106.1 | 126 | 911 | 1050 | 62 | 52. |
| 5 | 98.5 | 2.98 | 66 | 43.0 | 119.8 | 176 | 689 | 538 | 72 | 68. |
| 6 | 97.9 | 4.49 | 65 | 32.5 | 144.3 | 204 | 635 | 635 | 66 | 80 |
| 7 | 97.9 | 7.85 | 60 | 15.2 | 176.6 | 119 | 585 | 779 | 53 | 52. |
| 8 | 99.9 | 12.70 | 58 | 10.5 | 193.8 | 92.5 | 549 | 839 | 51 | 43. |
| 9 | 99.6 | 5.76 | 58 | 31.3 | 86.7 | 104.8 | 951 | 1411 | 46 | 61 |
| 10 | 100 | 8.22 | 66 | 19.2 | 92.6 | 101.1 | 1004 | 2046 | 60 | 74 |
| 11 | 100 | 12.42 | 70 | 18.6 | 83.2 | 90.3 | 1102 | 1175 | 86 | 99. |
| 12 | 97.0 | 5.49 | 51 | 14.0 | 207.1 | 137.8 | 508 | 560 | 45 | 43. |
| 13 | 97.5 | 2.04 | 58 | - | - | 242.2 | - | 551 | 71 | 65. |
| 14 | 97.8 | 4.04 | 57 | 33.3 | 148.2 | 178.4 | 618 | 655 | 78 | 62 |
| 15 | 95.7 | 4.77 | 52 | 49.0 | 76.1 | 337.5 | 897 | 786 | 77 | 81. |


| 16 | 100 | 10.20 | 53 | 13.1 | 58.6 | 147.6 | 1565 | 2868 | 36 | 59.0 | 3.67 | 74 | 6.01 | 65 |
| ---: | :---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: |
| 17 | 100 | 17.05 | 49 | 14.4 | 44.3 | 202.3 | 1912 | 3013 | 54 | 81.0 | 9.21 | 64 | 13.81 | 54 |
| 18 | 100 | 10.32 | 45 | 10.3 | 56.0 | 139.1 | 1693 | 2010 | 47 | 57.9 | 4.85 | 62 | 5.98 | 57 |
| 19 | 100 | 19.40 | 47 | 11.9 | 35.6 | 171.5 | 2362 | 3318 | 53 | 71.5 | 10.28 | 63 | 13.88 | 56 |
| 20 | 100 | 13.60 | 49 | 34.9 | 51.3 | 452.1 | 1302 | 944 | 62 | 78.5 | 8.43 | 61 | 10.68 | 55 |
| 21 | 96.4 | 2.33 | 39 | - | - | 373 | - | 414 | 53 | 55.3 | 1.23 | 50 | 1.29 | 49 |
| 22 | 96.5 | 3.49 | 45 | - | - | 454 | - | - | 77 | 72.3 | 2.69 | 50 | 2.52 | 51 |
| 23 | 98.7 | 5.61 | 46 | 89.7 | 76.5 | 425 | 675 | 700 | 87 | 69.8 | 4.88 | 49 | 3.92 | 54 |
| 24 | 100 | 8.82 | 43 | 75.9 | 89.2 | 443 | 680 | 765 | 83 | 75.2 | 7.32 | 47 | 6.63 | 49 |
| 25 | 100 | 15.24 | 43 | 46.3 | 56.1 | 476 | 1096 | 650 | 61 | 84.3 | 9.30 | 55 | 12.85 | 47 |
| 26 | 100 | 7.53 | 55 | 11.5 | 125.7 | 503 | 818 | 800 | 82 | 82.0 | 6.18 | 60 | 6.18 | 60 |
| 27 | 100 | 11.74 | 57 | 50.9 | 61.8 | 462 | 996 | 1135 | 81 | 74.6 | 9.51 | 62 | 8.76 | 64 |
| 27 | 59.6 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| 28 | 100 | 15.06 | 59 | 48.4 | 67.6 | 523 | 967 | 750 | 95 | 87.6 | 14.31 | 60 | 13.18 | 62 |
| 29 | 99.8 | 12.36 | 33 | 45.9 | 39.7 | 337.5 | 1311 | 1250 | 79 | 83.0 | 9.76 | 37 | 10.26 | 36 |

TABLE 3. Effects of $\mathrm{f}_{\mathbf{S}_{0}}$ on the Chloroform Extraction of Various Cured Polyester Resins

| Expt. <br> no. | Resin no |  | $\frac{\text { tyrene }}{f_{\mathrm{S}_{0}}}$ | $\underset{\text { (mole }}{\mathrm{C}_{\mathbf{S}}}$\%) | $\mathrm{w}_{0}$ <br> (mole <br> \%) | $\begin{aligned} & q_{0} \\ & \text { (mole } \end{aligned}$\%) | $\overline{\mathbf{M}}_{\text {SOL }}$ (from EGA) | $\bar{M}_{\text {SOL }}$ <br> (from <br> GPC) | Purity of polyester component (\%) |  | $W_{\text {IR }}$ <br> (mole <br> \%) | $\mathrm{q}_{\text {IR }}$ (mole \%) | $\begin{aligned} & \mathbf{w}_{\text {SN }} \\ & (\text { (mole } \\ & { }_{\mathrm{w})} \end{aligned}$ | ${ }^{q_{S N}}$ (mole \%) |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | wt \% | fraction |  |  |  |  |  | By IR | By SN |  |  |  |  |
| 4-1 | B(2)-5 | 39.1 | 0.738 | 98.5 | 2.99 | 57 | 619 | 500 | 78 | 66 | 2.33 | 62 | 1.96 | 65 |
| 4 | B(2)-5 | 50.0 | 0.814 | 98.0 | 3.64 | 53 | 911 | 1050 | 62 | 52 | 2.26 | 63 | 1.89 | 66 |
| 4-2 | B(2)-5 | 60.2 | 0.869 | 99.4 | 7.76 | 38 | 1626 | 1811 | 28 | 30 | 2.17 | 63 | 2.30 | 62 |
| 8-1 | B(2)-9 | 29.7 | 0.649 | 97.9 | 12.02 | 60 | 467 | 430 | 92 | 83 | 11.06 | 62 | 9.96 | 64 |
| 8 | B(2)-9 | 49.7 | 0.812 | 99.9 | 12.70 | 58 | 549 | 839 | 51 | 43 | 6.48 | 73 | 5.51 | 76 |
| 8-2 | B(2)-9 | 70.0 | 0.911 | 99.6 | 34.27 | 30 | 1237 | 4946 | 26 | 27 | 8.91 | 67 | 9.25 | 66 |
| 10-1 | B(9) | 5.0 | 0.290 | 90.4 | 32.43 | 30 | 948 | 1197 | 100 | 98 | 32.43 | 30 | 31.78 | 30 |
| 10-2 | B(9) | 15.0 | 0.578 | 100 | 6.04 | 72 | 852 | 667 | 97 | 96 | 5.86 | 73 | 5.77 | 73 |
| 10 | B(9) | 50.0 | 0.886 | 100 | 8.22 | 66 | 1004 | 2046 | 60 | 74 | 4.93 | 76 | 6.10 | 72 |
| 11-1 | B(15) | 5.0 | 0.369 | 100 | 17.87 | 61 | 1326 | 984 | 100 | 99 | 12.87 | 61 | 17.69 | 61 |
| 11-2 | B(15) | 15.0 | 0.662 | 100 | 9.89 | 75 | 918 | 1009 | 96 | 99 | 9.47 | 76 | 9.79 | 75 |
| 11-3 | B(15) | 30.7 | 0.831 | 100 | 10.78 | 73 | 1124 | 1100 | 88 | 99 | 9.49 | 76 | 10.67 | 73 |
| 11 | B(15) | 50.0 | 0.918 | 100 | 12.42 | 70 | 1102 | 1175 | 86 | 100 | 10.68 | 73 | 12.17 | 70 |
| 11-4 | B(15) | 68.0 | 0.961 | 100 | 12.92 | 69 | 1069 | 1200 | 83 | 90 | 10.72 | 73 | 11.59 | 71 |
| 20-1 | IPA | 28.9 | 0.697 | 100 | 11.28 | 54 | 846 | 600 | 90 | 100 | 10.15 | 56 | 11.28 | 54 |
| 20 | IPA | 50.4 | 0.853 | 100 | 13.60 | 49 | 1302 | 944 | 62 | 79 | 8.43 | 61 | 10.68 | 55 |
| 20-2 | IPA | 70.0 | 0.930 | 99.9 | 20.00 | 39 | 1638 | 3607 | 43 | 48 | 8.60 | 60 | 9.61 | 58 |


|  |  |
| :---: | :---: |
|  | $\underset{\sim}{\sim}$ |
|  |  |
|  |  |
|  |  |
|  |  |
|  |  |
|  | 呂 |
|  |  |
| $\underset{\sim}{\underset{\sim}{\sim}}$ |  |
| $\begin{gathered} \dot{\infty} \\ \underset{\sim}{\infty} \end{gathered}$ | 웅응으응으으응응응 |
| $\begin{aligned} & \text { H্N } \\ & \text { مٌ } \end{aligned}$ |  |
| $\underset{\sim}{\underset{\sim}{c}}$ |  |
| \# |  |
| $\overrightarrow{\mathfrak{\mu}}$ |  |

conversion of fumarate double bond qo was calculated from the soluble part of the cured polyester resin, $W_{0}$, as presented in the previous paper [9]. The soluble part, W , of the polyester resin is given by

$$
\begin{equation*}
\mathrm{W}=\sum_{\mathrm{x}=1}^{\infty} \mathrm{W}_{\mathrm{x}}(1-\mathrm{q})^{\mathrm{x}} \tag{1}
\end{equation*}
$$

where $q$ is the conversion of fumarate double bond, $x$ is the number of units in the polyester chain, and $W_{x}$ is the weight fraction of molecule containing $x$ units.

The values of $q_{0}$ apparently vary with the chemical structure and composition of the starting unsaturated polyester resins.

The relationships between $f_{S_{0}}$ and $q_{0}$ are shown in Figs. 1 and 2 for Bisphenol-type resins and for Iso-type and G-type resins, respectively, where the effect of chemical characteristics of the unsaturated polyester resins on $q_{0}$ at the same levels of $f_{S_{0}}$ are exemplified. As $\mathrm{f}_{\mathrm{S}_{0}}$ increases, $\mathrm{q}_{0}$ increases up to $\mathrm{f}_{\mathrm{S}_{0}}=0.6$; the highest $q_{0}$ is attained at $f_{S_{0}}=0.6 \sim 0.7$. At the levels higher than this region, $q_{0}$ decreases. This observation is not in accord with the results by other investigators [ $1,2,6,7,8,11$ ].

Figures 1 and 2 show that the effect of $M_{0}$ on $q_{0}$ is very distinctive. In comparison, at the region of $\mathrm{f}_{\mathrm{S}_{0}}=0.6 \sim 0.7$ where $q_{0}$ reaches its


FIG. 1. Relationship between $f_{S_{0}}$ and $q_{0}$ for Bisphenol-type resins.


FIG. 2. Relationship between $\mathrm{f}_{\mathrm{S}_{0}}$ and $\mathrm{q}_{0}$ for Iso-type and G-type resins.
peak, the larger the $\overline{\mathrm{M}}_{0}$, the higher the $\mathrm{q}_{0}$. For instance, $\overline{\mathrm{M}}_{0}$ for Bisphenol-type resins increased with increasing length of the polyoxypropylene unit attached to Bisphenol $A$. The increase in $\bar{M}_{0}$ enhances the flexibility of the cured resin, which seems to be favorable for raising the conversion of fumarate double bond. The results for G-type and iso-type resins in Fig. 2 show the same relationships between $\mathrm{M}_{0}$ and $\mathrm{q}_{0}$ as that for Bisphenol-type resins. The type of dibasic acid used as the modifier has a large effect on $q_{0}$. The adipic acid modification gave the highest $q_{0}$, the isophthalic acid modification gave intermediate values of $q_{0}$, and the phthalic acid modification and the unmodified resin having the smallest in $\bar{M}_{0}$ gave the lowest $q_{0}$. These results suggest that the network structure of copolymer may affect distinctively the reactivity of fumarate double bonds with styrene.

The acid number and hydroxyl number of the extracted resin were determined. If the extracted polymer consists purely of unsaturated polyester resin, the number-average molecular weight can be determined from the endgroup analysis. The effects of $\mathrm{f}_{\mathrm{S}_{0}}$ on the molecular weight of the soluble part of the polyester resin, $\overline{\mathrm{M}}_{\mathrm{SOL}}$, is shown in Table 3. The molecular weight of the soluble portion should decrease
with conversion of the fumarate double bond according to the present theory. $\bar{M}_{\text {SOL }}$ decreases with the $q_{0}$ up to $f_{S_{0}}=0.6 \sim 0.7$, but it increases in the region above $f_{\mathrm{S}_{0}}=0.7$. The increase in $\overline{\mathrm{M}}_{\mathrm{SOL}}$ at the higher $f_{S_{0}}$ does not agree with the general observations by other investigators that the conversion of fumarate double bonds increases with $\mathrm{f}_{\mathrm{S}_{0}}$. The effects of $\mathrm{f}_{\mathrm{S}_{0}}$ on the molecular weight of the soluble part determined by gel-permeation chromatography are also shown in Table 3. The results show the same relationship as the results from endgoup analysis. The sharp increase in $\overline{\mathrm{M}}_{\text {SOL }}$ at the higher levels of $\mathrm{f}_{\mathrm{S}_{0}}$ are more pronounced.

It is predicted from these results that the production of the styrene homopolymer may occur at higher $\mathrm{f}_{\mathrm{S}_{0}}$, because the amount of uncrosslinked soluble polyester resin is more than that expected. Funke et al. [4] raised the question of whether free chains of polystyrene are formed in addition to the crosslinked copolymer chain because they observed that turbidity sometimes developed after curing of the polyester chain. However, they did not find evidence for the presence of the styrene homopolymer by liquid-liquid distribution chromatography of the addition polymers isolated from the hydrolysis product of the cured resin. Katz and Tobolsky [12] have predicted the formation of the styrene homopolymer in the nontransparent resin obtained after the cure.

The isolation of styrene homopolymer is an important point in the present study. A typical Bisphenol-type polyester resin was used. A $0.2550-\mathrm{g}$ portion of the extracted resin from the cured resin of experiment 3 in Table 1 was analyzed by elution chromatography with a silica gel-packed column. First the column was eluted with methanol and subsequently with chloroform, The resin from the methanolsoluble fraction was $0.1917 \mathrm{~g}(75.18 \mathrm{wt} \%)$ and the resin from the chloroform-soluble fraction was 0.0425 g ( $16.67 \mathrm{wt} \%$ ). The residual $8.15 \mathrm{wt} \%$ of the resin was absorbed strongly on the silica gel and not extracted by further elution with chloroform. The chemical structure was analyzed by infrared spectroscopy for each fraction. The results are shown in Fig. 3, and the spectra of the standard unsaturated polyester resin [Resin $B(2)-4]$ and polystyrene are shown in Fig. 4. The infrared spectrum for the methanol-soluble fraction is the same as that of the standard polyester resin with the exception of a few bands, including a band at $690 \mathrm{~cm}^{-1}$ due to the styrene unit. The infrared spectrum for the chloroform-soluble fraction is the same as that for polystyrene with the exception of the very weak absorption at $1260 \mathrm{~cm}^{-1}$ which appears as a strong absorption in the infrared spectrum of the

FIG. 3. Infrared spectra for (-) the methanol-soluble fraction and (--) the chloroform-soluble
fraction.



FIG. 5. Distribution curves by the gel permeation chromatography: (1) polyester resin $B(2)-4$; (2) extracted resin; (3) methanol-soluble fraction; (4) chloroform-soluble fraction.
standard polyester resin. Elemental analysis for $C$ and $H$ of the chloroform-soluble fraction showed: $\mathrm{C}, 91.8 \% ; \mathrm{H}, 7.8 \%$ (calcd for $\mathrm{C}_{8} \mathrm{H}_{8}$ : C, $92.26 \% ; \mathrm{H}, 7.7 \%$ ). Each fraction was analyzed by gel-permeation chromatography (Fig. 5). Distribution curves were compared with

TABLE 4. Number-Average Molecular Weight

|  | $\overline{\mathbf{M}_{\mathbf{n}}}$ |  |  | By gel permeation <br> chromatography | By endgroup <br> analysis |
| :--- | :--- | :--- | :---: | :---: | :---: |
| Starting polyester resin <br> $\mathrm{B}(2)-4$ <br> Extracted resin | 2351 | 2794 |  |  |  |
| Methanol-soluble fraction | 1284 | 885 |  |  |  |
| Chloroform-soluble fraction | 430 | - |  |  |  |

that of the starting polyester resin, $\mathrm{B}(2)-4$. The number-average molecular weight determined by gel-permeation chromatography and endgroup analysis are shown in Table 4. The molecular weight of the chloroform-soluble fraction is much higher than that for the methanol fraction. These results provide support for the supposition that styrene homopolymer is produced as a by-product in copolymerization of styrene with unsaturated polyester resins. The methanol-soluble fraction contains some styrene units, although it is still unknown whether it is due to styrene homopolymer or polystyrene units linked to the polyester chain.

On assuming that all the polystyrene component in the extracted polyester resin is present as homopolymer, the content of the polyester resin was determined by infrared spectroscopy. The calibration curves were obtained by plotting the percent of the area of the band at $1720 \mathrm{~cm}^{-1}$ of the total areas of the bands at $1720 \mathrm{~cm}^{-1}$ and $690 \mathrm{~cm}^{-1}$ against the weight percent of the polyester resin in the resin mixture of polyester resin and polystyrene. The band at $1720 \mathrm{~cm}^{-1}$ is used as a specific band for polyester resin and the band at $690 \mathrm{~cm}^{-1}$ is used as a specific band for polystyrene. Several typical calibration curves are shown in Fig. 6.

Another method to determine the purity of polyester resin in extracted resin is the analysis of saponification number. The purity of polyester resin determined by the infrared spectroscopy and the saponification number decrease with $\mathrm{f}_{\mathrm{S}_{0}}$, as shown in Table 3. The infrared spectroscopy and the saponification number method give nearly the same results. At $\mathrm{f}_{\mathrm{S}_{0}}$ higher than $0.6-0.7$, the purity of polyester resin decreases. The change is quite pronounced for resins


FIG. 6. Calibration curves by the infrared spectroscopy for the weight \% of unsaturated polyester resin in the resin mixture of unsaturated polyester resin and polystyrene.
having low $\bar{M}_{0}$, such as resins $B(2)-5$ and $G-3$, but it is moderate for resin having large $\bar{M}_{0}$, such as resins $B(15)$ and G-9. The amount of the extracted polyester resin was corrected for by the infrared spectroscopy or the saponification number method, and the conversion of fumarate double bond was recalculated by using the corrected values of the extracted polyester resin. $W_{I R}$ and $W_{S N}$ are the corrected soluble portion of polyester resin and $q_{I R}$ and $q_{S N}$ are the corrected conversion of fumarate double bond, where the subscripts denote the method of correction.

The effects of $f_{S_{0}}$ on $W_{I R}$ or $W_{S N}$ and $q_{I R}$ or $q_{S N}$ are shown in Table 3, and the relationships between $f_{S_{0}}$ and $q_{I R}$ or $q_{S N}$ are shown in Figs. 7-10. With increasing $f_{S_{0}}, W_{I R}$ or $W_{S N}$ decrease and $q_{I R}$ or $q_{S N}$ increase, and both the $W$ and $q$ level off at the higher regions of $f_{S_{0}}$. The values of $q_{I R}$ or $q_{S N}$ for the unsaturated polyester resins


FIG. 7. Relationship between $f_{S_{0}}$ and $q_{\mathbb{I} R}$ for Bisphenol-type resins.
having high $\overline{\mathrm{M}}_{0}$ levels off at the lower levels of $\mathrm{f}_{\mathrm{S}_{0}}$, but the values for the resins having low $\overline{\mathrm{M}}_{0}$ increase at higher levels of $\mathrm{f}_{\mathrm{S}_{0}}$. From these results the effect of the chemical structure of unsaturated polyester resin on the conversion of fumarate double bond can be compared by $q_{I R}$ or $q_{S N}$ at the region where the values of $q_{I R}$ or $q_{S N}$ are in plateau. The corrected values, $q_{I R}$ of $q_{S N}$, are compared at $50 \pm 0.5 \mathrm{wt} \%$ of the initial concentration of styrene for all polyester resins as shown together with $q_{0}$ in Table 2.

In the Bisphenol-type resins all the polyester resins modified by neopentylglycol, propylene glycol, hydrogenated Bisphenol A, $\beta$ hydroxyethyl terephthalate, succinic acid, and adipic acid gave the same levels of corrected values of the conversion of fumarate double bond, i.e., $q_{I R}$ or $q_{S N}=60 \sim 70$ mole $\%$. However, if the resin is modified by a polyoxypropylene unit adducted to Bisphenol A, the conversion of fumarate double bond increases up to $q_{I R}$ or $q_{S N}=$ $73 \sim 76$ mole \%. For the standard Bisphenol-type resin, the effect


FIG. 8. Relationship between $\mathrm{f}_{\mathrm{S}_{0}}$ and $\mathrm{q}_{\mathrm{I} R}$ for Iso-type and G-type resins.


FIG. 9. Relationship between $f_{S_{0}}$ and $q_{S N}$ for Bisphenol-type resins.


FIG. 10. Relationship between $\mathrm{f}_{\mathrm{S}_{0}}$ and $\mathrm{q}_{\mathrm{SN}}$ for Iso-type and G-type resins.
of the number-average degree of polyesterification $\bar{x}$ on the conversion of fumarate double bond is shown in Fig. 11. At $\bar{x}<5, q_{0}$ increases slightly with $\bar{x}$ but $q_{I R}$ and $q_{S N}$ are located at the same level. At $\bar{x}>5, q_{0}, q_{R^{\prime}}$, and $q_{S N}$ all decrease with $\bar{x}$.

In the polyester resin of propylene glycol fumarate, the fumaric acid is modified with adipic acid, isophthalic acid, and phthalic acid anhydride. The corrected conversion of fumarate double bond for these modified resins follows the order of adipic $>$ isophthalic $>$ phthalic $>$ unmodified, ranging from 60 to 45 mole $\%$. The polyester resin prepared from chlorendic acid anhydride (Resin HETA) gives the lowest conversion of fumarate double bonds.

The crosslinking of unsaturated polyester resins with styrene proceeds by a radical process to form a three-dimensional network. In the early stages of the copolymerization the polymer is an alternating copolymer. Before the formation of a highly crosslinked network, the resin is soft, and there are some spaces for styrene monomer to react with unreacted fumarate double bond in the network. After the network becomes rigid and compact, diffusion of the styrene


FIG. 11. Relationship between $\bar{x}$ and $(0) q_{0},(\Delta) q_{I R}$, or $(\square) q_{S N}$ for Bisphenol-type resins.
monomer to the fumarate double bonds in the rigid network is very difficult, but the styrene monomer can react with either polystyrene radicals linked to the polyester chain or free polystyrene radicals newly generated outside the network. The latter reaction gives the styrene homopolymer which may be formed preferentially at the higher levels of $f_{S_{0}}$, especially at the later stages of copolymerization. The formation of the styrene homopolymer is unfavorable in polyester resin having large $\mathrm{M}_{0}$. The network formed is so loose and spacious that contact of the styrene monomer with the fumarate double bonds or the polystyrene radical linked to the polyester resin is easy. The bulky group such as chlorine group in the Het acid-type resin hinders the styrene radical to attack the fumarate double bonds. The phthalate resins and the propylene glycol fumarate polyester resin produce a compact crosslinked network at low conversion of fumarate double bond.

According to Flory [ 10], the effective number of chains in a real network is given by

$$
\begin{equation*}
\nu_{\mathrm{e}}=\nu\left(1-2 \overline{\mathrm{M}}_{0} / \overline{\mathrm{M}}_{\mathrm{n}}\right) \tag{2}
\end{equation*}
$$

or

$$
\begin{equation*}
\nu_{\mathrm{e}}=\nu(1-2 / \overline{\mathrm{x}}) \tag{3}
\end{equation*}
$$

where $\nu$ is the number of crosslinked units, $\overline{\mathrm{M}}_{0}$ is the molecular weight per crosslinked unit, and $\bar{M}_{n}$ is the molecular weight of the starting polyester resin. At a fixed molecular weight for $\overline{\mathrm{M}}_{0}, \nu_{e}$ will increase with $\bar{M}_{n^{*}}$. The unsaturated polyester resin providing a higher effective crosslinking density forms a complete network before all the fumarate double bond is reacted with styrene. The higher the crosslinking density, the more compact the network of the crosslinked polymer. As a result, the conversion of fumarate double bond is lowered. At a fixed molecular weight $\bar{M}_{n}, \nu_{e}$ will decrease with $\bar{M}_{0}$. The polyester having a large $\overline{\mathbf{M}}_{0}$ produces low-density networks even if $\bar{M}_{n}$ is relatively large.

## ACKNOWLEDGMENTS

The authors wish to express their thanks to Miss Fumiko Sugimoto for her experimental assistance. Appreciation is also extended to Professor T. Saegusa of Kyoto University for his helpful discussion.

## REFERENCES

[ 1] W. Funke, W. Gabhardt, H. Roth, and K. Hamann, Makromol. Chem., 28, 17 (1958).
[2] W. Funke, H. Roth, and K. Hamann, Kunststoffe, 51, 75 (1961).
[3] W. Funke and H. Janssen, Makromol. Chem., 50, 188 (1961).
[4] W. Funke and K. Hamann, Mod. Plast., 39, 147, 148, 150, 226 (1962).
[5] K, Hamann, W. Funke, and H. Gilch, Angew. Chem., 71, 596 (1959).
[6] N. A. Ghanem, Makromol. Chem., 36, 109 (1960).
[7] M. Bohdanecky, J. Mleziva, A. Sternschuss, and V. Zvonar, Makromol. Chem., 47, 201 (1961).
[8] K. Demmler, Kunststoffe, 56, 606 (1966).
[9] K. Sakaguchi, J. Macromol. Sci.-Chem., A8, 477 (1974).
[10] P. J. Flory, Principles of Polymer Chemistry, Cornell Univ. Press, Ithaca, N. Y., 1953.
[11] W. Funke and R. Feinauer, Makromol. Chem., 49, 52 (1961).
[12] D. Katz and A. V. Tobolsky, J. Polym. Sci. A, 2, 1587 (1964).

Accepted by editor June 28, 1975
Received for publication October 27, 1975


[^0]:    *Present address: Kao Soap Co., Ltd., 1-1 Kayabacho, Nihonbashi, Chuoku, Tokyo 103 Japan.

